# 

EXCELLENCE IN PUMPS

**Brass Engineering Slurry Pipeline Seminar, Bhubaneswar, day1** 

**Feluwa Presentation:** Piston Diaphragm Pumps for pipeline slurry transfer: When and why to apply piston diaphragm pumps

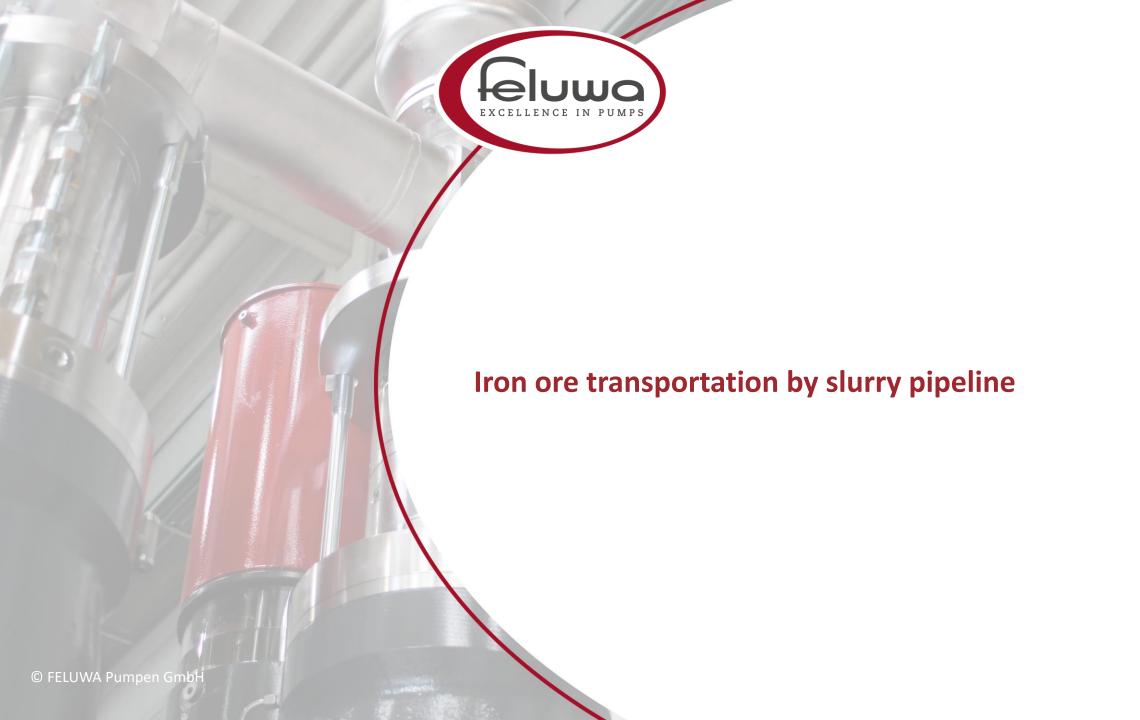
> By: Hein Krimpenfort Key Account Manager, Feluwa Pumps

© FELUWA Pumpen GmbH

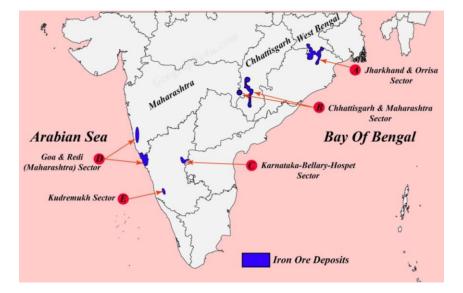


- Purpose of this presentation:
- 1) Introduce piston diaphragm pump technology
- 2) Proof that piston diaphragm pumps can be a feasible alternative for multistage centrifugal pumps
- 3) Present differences pumping concentrate or tailings slurry (there aren't any!)





- Long distance transportation of iron ore
  - Demand for iron/steel worldwide is booming
    - Around 8% of the world's total iron ore deposits are located in India
    - Iron ore deposits can be found in Karnataka, Orissa, Chhattisgarh, Goa and Jharkand
    - Enormous quantities of Iron ore needs to be transported from mines to processing plants





- Long distance transportation of iron ore
  - Options
    - Truck
      - Approx. 30% of iron ore transport in India
      - High environmental impact
      - Operating cost per ton per km is 7,5 INR
    - Train
      - Approx. 60 to 70% of iron ore transport in India
      - Medium environmental impact
      - Operating cost per ton per km is 4,75 INR
    - Pipeline
      - Approx. 5 to 10% of iron ore transport
      - Low environmental impact
      - Operating cost per ton per km is 0,35 INR







D FELUWA Pumpen GmbH



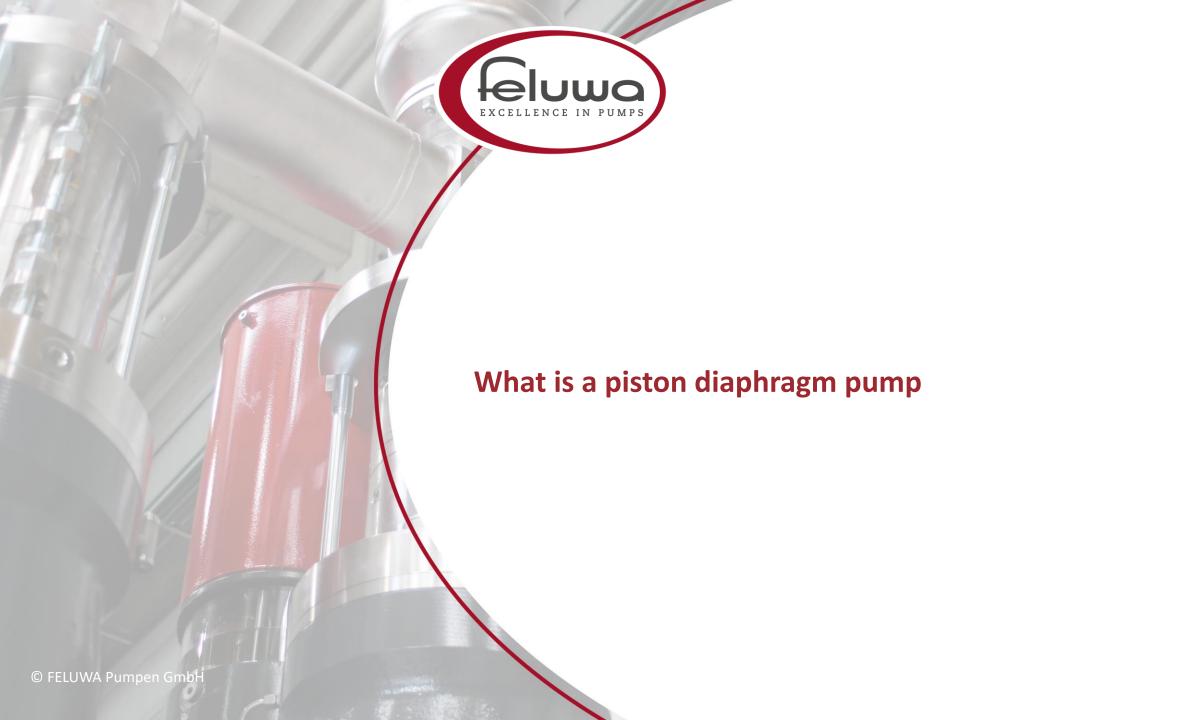
- Long distance transportation of iron ore
  - Pipelines:
    - Cheapest way of transporting iron ore
    - Lowest environmental impact
    - Are the preferred transporting method



- Long distance transportation of iron ore
  - Concentrate pipelines
    - Proven technology
    - Thousands of kilometers of pipelines are in operation, worldwide
    - Hundreds of pumps are in service as prime mover
    - Type of pump is piston diaphragm



- Long distance transportation of iron ore
  - Iron ore slurry pipelines in India
    - Number of operating pipelines : 3
    - Number of pipelines under construction : 5
    - Number of pipelines being designed : 15 to 20



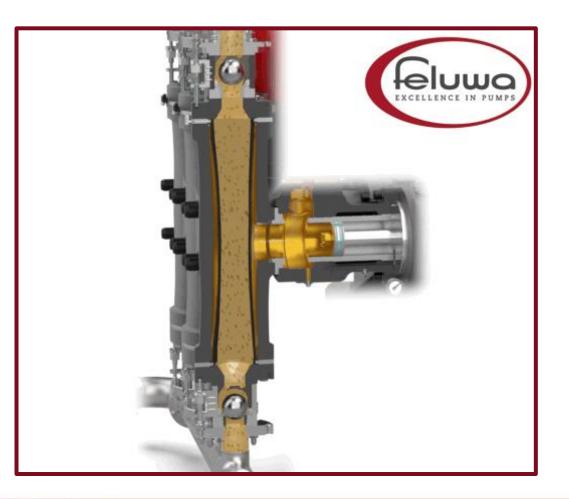
- What is a piston diaphragm pump:
  - A piston diaphragm pump is a positive displacement pump in which the main moving parts run in hydraulic oil and are separated from the fluid by means of an elastomere.
  - The only wearing parts in a piston diaphragm pump are the suction and discharge valves



- What is a piston diaphragm pump:
  - Piston diaphragm pumps are being used in the mining industry since more than 60 years
- Thousands of piston diaphragm pumps have been installed for various applications
- Piston diaphragm pumps are proven technology



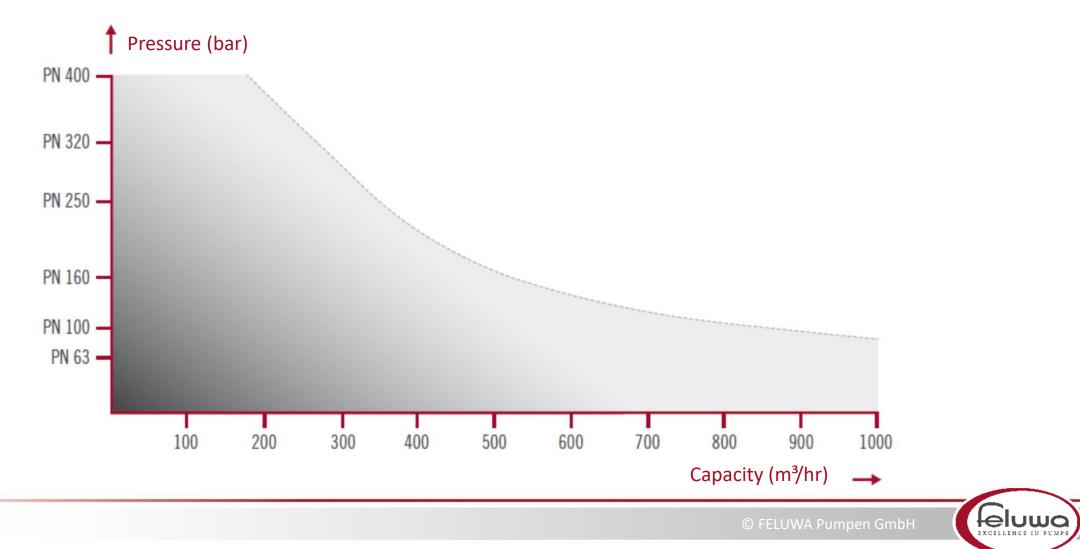
• What is a piston diaphragm pump:



© FELUWA Pumpen GmbH



• Pump range:



• What is a piston diaphragm pump:



FELUWA Pumpen GmbH





# Piston Diaphragm Pumps can be a feasible alternative for multistage centrifugal pumps

© FELUWA Pumpen GmbH

- Piston Diaphragm Pumps can be a feasible alternative for multistage centrifugal pumps:
  - Typical example

•

- Pipeline distance
  - Pipeline capacity
- Discharge pressure
- Price of power
- Number of pumps
  - Centrifugal
- : 6 + 6 in series

: 18 km (irrelevant)

: 6 INR/kWh (US\$ 0,08)

: 1.000 m<sup>3</sup>/hr

: 40 bar





- Piston Diaphragm Pumps can be a feasible alternative for multistage centrifugal pumps:
  - Typical example ٠
    - Pipeline distance : 18 km (irrelevant) •
    - Pipeline capacity •
    - Discharge pressure •
    - •

: 40 bar

: 6 INR/kWh (US\$ 0,08)

: 1.000 m<sup>3</sup>/hr

- Price of power
- Number of pumps •
  - Piston diaphragm : 2 + 1 •





- Feasibility comparison
  - Investment/CAPEX

Investment			
		Centrifugal	PD Pump
Required data		Metso:Ototec	DGK400
Number of required operating + standby pumps		12	3
Price per pump	in \$	150.000,00	1.000.000,00
Calculation			
Total system price	in \$	1.800.000,00	3.000.000,00
Difference in investment	in \$		- 1.200.000,00

#### • Feasibility comparison

#### • Power/OPEX

Power consumption			
		6 + 6	2 + 1
Required data		Centrifugal	PD Pump
Pressure	bar	40	40
Capacity	m³/hr	1000	1000
Price per kW hr (6 Rupees per kWh)	in \$	0,08	0,08
Operating hours	per year	8700	8700
Mechanical efficiency	in %	65	95
Calculation			
Absorbed power	in kW	1709	1170
Hourly power cost	in \$	136,75	93,57
Annual power cost	in \$	1.189.743,59	814.035,09
Difference in power consumption	in \$		375.708,50

- Feasibility comparison
  - Wearing parts/OPEX

Spare parts costs			
Required data		Centrifugal	PD Pump
Parts consumption in % of purchase price (assumed)	in %	50	5
Calculation			
Annual pump spare parts cost operating pumps	in \$	450.000,00	99.000,00



- Feasibility comparison
  - Labour/OPEX

Labour costs			PD Pump
Required data		Centrifugal	
Number of required pumps		12	3
Maintenance man hours per year per pump (assumed)	hrs	100	50
Labour costs per hours (assumed)	in \$	30	30
Calculation			
Labour maintenance costs per year for system	hrs	36.000,00	4.500,00
Difference in maintenance cost	in \$		31.500,00

FELUWA Pumpen GmbH

#### • Feasibility comparison

#### • Summary

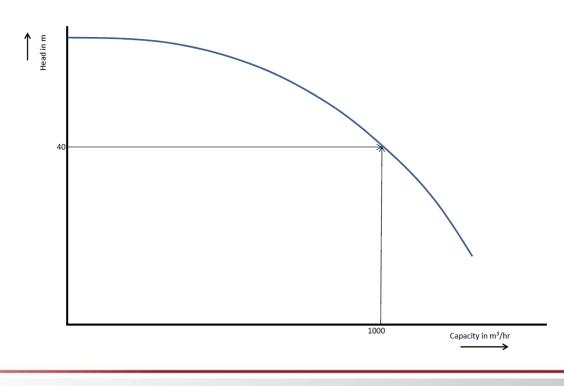
Summary			
		Centrifugal	PD Pump
Annual power consumption		1.189.743,59	814.035,09
Spare parts costs	in \$	450.000,00	99.000,00
Labour costs	in \$	36.000,00	4.500,00
Total operating costs	in \$	1.675.743,59	917.535,09
Difference of total operating costs per month	in \$	63.184,04	
Total investment	in \$	1.800.000,00	3.000.000,00
Amortization period of diffence in investment	in month	s	18,99
	in years		1,58

FELUWA Pumpen GmbH

- Feasibility comparison
- Conclusion
  - Depending on
    - Pressure
    - Price of power
    - Abrasivity of the slurry
  - Piston diaphragm pumps can be a feasible alternative for centrifugal pumps

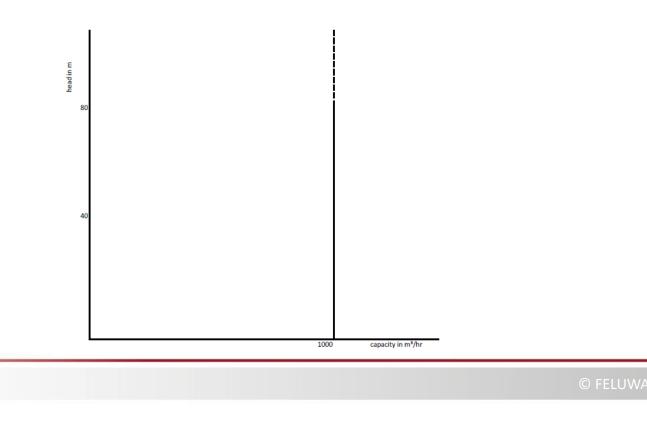


- Technical comparison
- In a centrifugal pump capacity is pressure dependent
  - If the pressure increases
  - The capacity decreases



- Technical comparison
- In a centrifugal pump capacity is pressure dependent
  - If the pressure increases
  - The capacity decreases
  - There is a considerable risk of clogging the pipeline

- Technical comparison
- In a piston diaphragm pump capacity is not pressure dependent
  - If the pressure increases
  - The capacity remains the same





- Technical comparison
- In a piston diaphragm pump capacity is not pressure dependent
  - If the pressure increases
  - The capacity remains the same
  - The risk of clogging a pipeline is minimal



• NOTE:

#### A pump does not generate/create/make pressure, it does not

A pump merely overcomes a back pressure



FELUWA Pumpen GmbH

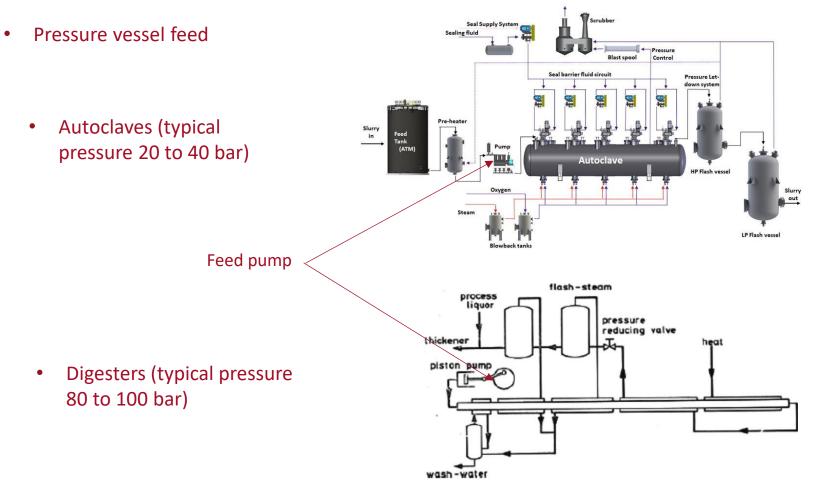
- A pump does not generate/create/make pressure
- Applications for piston diaphragm pumps in the mining and metallurgical industry
  - Pressure vessel feed
    - Autoclaves in gold, copper, nickel, etc
    - Digesters in bauxite
  - Mine dewatering
    - Clean water + sludge
    - Dirty water
  - Pipeline transfer
    - Tailings
    - Concentrate



- Where does pressure come from
- Pressure vessel feed
  - A vessel is pressurized in order to create an atmosphere in which the concentrate is liberated from the ore (in addition to high temperatures, high acidity)
    - In order to transfer ore into the vessel, the pump has to be able to overcome the pressure in the vessel



• Where does pressure come from



FELUWA Pumpen GmbH

- Where does pressure come from
- Pressure vessel feed
  - Note:
    - If the pressure in the vessel is 30 bar, the pump will deliver a pressure of slightly more than 30 bar, even if the pump is designed for 40 bar (or more)
    - The pump will produce pressure to overcome the back pressure from the vessel, not more

: 3,2 kg/dm<sup>3</sup>

:NA

- Where does pressure come from
- Pressure vessel feed, example
  - Location :
  - Customer
  - Type and qty of pumps : 8 x Feluwa TGK135
  - Capacity per pump
  - Type of slurry
  - SG of solids
  - Solids concentration : 20%
  - Length of pipeline : NA
  - Static head : NA
  - Slurry velocity
  - Discharge pressure
- : 38 bar (autoclave pressure)



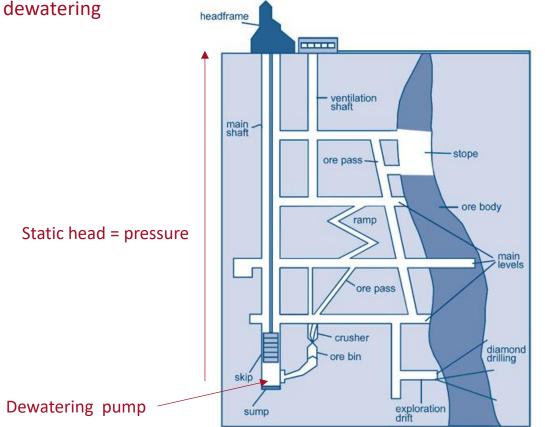




- Where does pressure come from
- Mine dewatering
  - In an underground mine, process and groundwater needs to be pumped to surface
    - The dewatering pump has to be able to overcome the static back pressure created by the column of water from the pump to surface (multiplied by the SG of the slurry)



- Where does pressure come from
- Mine dewatering ٠



Static head	= 500 m
SG of mine water	= 1,1 kg/dm <sup>3</sup>
Required pressure	= 55 bar

Static head

SG of mine water

**Required** pressure

= 300 m
= 1,0 kg/dm <sup>3</sup>

= 30 bar

- Where does pressure come from
- Mine dewatering
  - Note:
    - If static head is 300 meters (@ SG of 1,0 kg/dm<sup>3</sup>), required discharge pressure will be 30 bar, (even if the pump is designed for 40 bar, or more)
    - The pump will produce pressure to overcome the back pressure from static head, not more

- Where does pressure come from
- Mine dewatering, example
  - Location : Turkey
  - Customer
  - Type and qty of pumps : Feluwa DGK400
  - Capacity per pump
  - Type of slurry
  - SG of solids
  - Solids concentration
  - Length of pipeline : 8
  - Static head
  - Slurry velocity

: 1,05 kg/dm³

: Dirty mine water

: 5%

: Esan

: 250 m³/hr

- : 800 m (vertical)
- : 85 bar
- : 2,5 m/sec
- Design pump pressure : 100 bar (only static head)



- Where does pressure come from
- Slurry pipeline transfer
  - In a pipeline, the pump has to overcome back pressure created by
    - Static head
      - If the difference in elevation between the start and the end of the pipeline
    - Friction losses
      - Friction losses created by the slurry/meter need to be multiplied by the pipeline length
  - In order to transfer the slurry from the beginning of the pipeline to the end, the pump needs to overcome the total back pressure created by the pipeline (static head + friction losses)



- Where does pressure come from
- Slurry pipeline transfer
  - Static head :
    - In case difference in altitude from start till the end of the pipeline is 300 meters, the back pressure that the pump needs to overcome is 300 x the SG of the slurry
    - In case SG of slurry is 1,6 kg/dm<sup>3</sup>, static head will be 48 bar



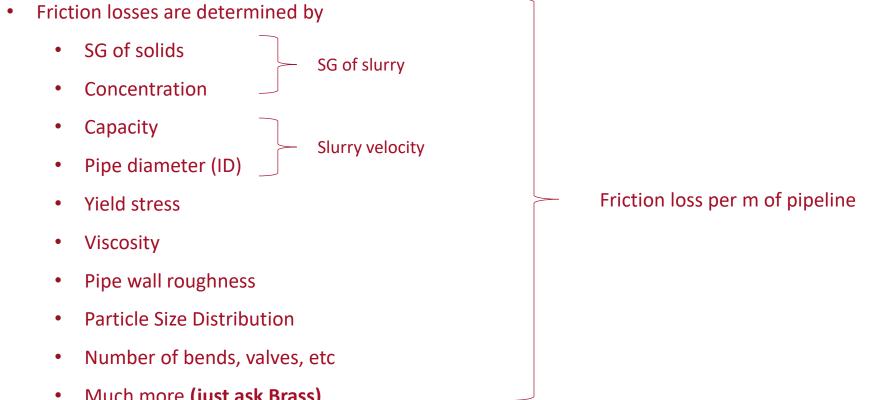


- Where does pressure come from
- Slurry pipeline transfer
  - Friction losses:
    - Depend on various factors and need to be determined by specialized slurry pipeline engineering companies





- Where does pressure come from
- Slurry pipeline transfer ٠



Much more (just ask Brass)

- Slurry pipeline transfer
- Note 1:
  - Pressure
    - Type of slurry (concentrate or tailings) is not a criteria
    - For friction loss calculation, "slurry is slurry"
    - For a piston diaphragm pump, "slurry is slurry"

- Slurry pipeline transfer
- Note 2:
  - Pressure
    - In case pipeline goes down hill, static head is negative
    - In case friction losses exceed negative static head, additional pump pressure is required to transfer slurry down hill

- Slurry pipeline transfer
- Note 3
  - Significance of SG of solids for piston diaphragm pumps:
    - Typically, SG of solids of tailings is 2,3 to 3,0 kg/dm<sup>3</sup>
      - Typically, the SG of tailings slurry is 1,3 to 2,0 kg/dm<sup>3</sup> (depending on solids concentration)
    - Typically, SG of solids of concentrate is 2,5 to 5,5 kg/dm<sup>3</sup>
      - Typically, the SG of concentrate slurry is 1,7 to 2,3 kg/dm<sup>3</sup> (depending on solids concentration)
  - For a piston diaphragm pump the SG of the slurry determines the NPSH required
    - A high SG of slurry, requires a higher NPSHr



- Slurry pipeline transfer
- Note 3
  - Significance of SG of solids:
    - A high SG of slurry, requires a higher NPSHr

		Per	Data S			
	Project		Brass Seminar_I	REVA00	)	
	Type of F	Pump	TGK 500 - 3 D	S 350	SAP#: D000	0219
Note				Note		Re
1	Operating Conditions			Performance		
2	Discharge Pressu	re	150,0 bar(g)		Rated Capacity	349,55 m <sup>3</sup> /h
3	Suction Pressure	(regiured for water)	0,0 bar(g)		Minimum Capacity	111,56 m³/h
4		Fluid			NPSHr (water column)	<mark>8,5 m</mark>
5	Density		1,10 g/cm <sup>3</sup>	$\rightarrow$	Mean Piston Speed	0,78 m/s
6	Viscosity		500.0 cP		Mechanical Efficiency	94,7 %
7	Particle Size		0,50 mm		Volumetric Efficiency	91,0 %
8	Temperature		20 °C		Maximum Power Consumption	1538,4 kW
9	Construction			Motor Torque	9795,0 Nm	
0		Size &	Rating		Minimum Speed	15 spm
1	Suction Nozzle	16" CI.150-RF	-		Maximum Speed	47 spm
2	Discharge Nozzle	16" CI.1500-RT.	I		Differential Pressure	150,0 bar
13	Flush Nozzle (S +	D) 4" CI.150-RF + 4" CI	.1500-RTJ		Piston Displacement	45,40 liter

4	eluwa	Da	ata Shee	et	
1.2	CELLENCE IN PUMPS	Performanc	e Curve SI	units [bar]	
	Project	Brass Ser	ninar_REVA0	0	
	Type of Pum	p TGK 50	0 - 3 DS 350	SAP#: D00	0219
Note			Note		R
1	Oper	ating Conditions		Performa	nce
2	<b>Discharge Pressure</b>	150,0	bar(g)	Rated Capacity	349,55 m <sup>3</sup> /h
3	Suction Pressure (regi	ured for water) 0,4	bar(g)	Minimum Capacity	111,56 m <sup>o</sup> /h
	Fluid			NPSHr (water column)	13,3 m
	Density	2,00	g/cm <sup>3</sup>	Mean Piston Speed	0 <del>,78</del> m/s
ŝ	Viscosity	500.0	°P	Mechanical Efficiency	94,7 %
	Particle Size	0,50	mm	Volumetric Efficiency	91,0 %
	Temperature	20 5	°C	Maximum Power Consumption	1538,4 kW
)	Construction			Motor Torque	9795,0 Nm
)		Size & Rating		Minimum Speed	15 spm
	Suction Nozzle	16" CI.150-RF		Maximum Speed	47 spm
	Discharge Nozzle	16" CI.1500-RTJ		Differential Pressure	149,6 bar
j.	Flush Nozzle (S + D)	4" CI.150-RF + 4" CI.1500-RTJ		Piston Displacement	45,40 liter

- Slurry pipeline transfer
- Note 4
  - Critical velocity:
    - SG of solids determines the critical/precipitation velocity of a slurry in the pipeline
    - Particle Size Distribution plays an important role in determining the critical velocity
    - The higher the SG of solids is, the higher the slurry velocity in the pipeline (to prevent settling of these solids
    - In order to achieve a higher velocity, the diameter of the pipeline needs to be decreased
    - The higher the slurry velocity in the pipeline, the higher the friction losses will be

- Slurry pipeline transfer
- Slurry pipeline transfer, example tailings ٠
  - Location •

٠

- Customer
- Type and qty of pumps ٠
- Capacity per pump ٠
- SG of slurry ٠
- Length of pipeline ٠
- Static head ٠
- Slurry velocity ٠
- Static head ٠
- Friction losses ٠
- : 4.500 kPa **Design pump pressure** ٠

: Minera Boleo

: Mexico

- : 4 x Feluwa QGK500
- : 750 m³/hr
- : 1,7 kg/dm<sup>3</sup>
- : 6 km
- : 200 m
- : 1,8 m/sec



: 1.100 kPa







- Slurry pipeline transfer
- Slurry pipeline transfer, example concentrate
  - Location
  - Customer
  - Type and qty of pumps
  - Capacity per pump
  - SG of solids
  - Length of pipeline
  - Static head
  - Slurry velocity
  - Static head
  - Friction losses
  - Design pump pressure

: Kenmare

: Mozambique

- : 3 x Feluwa TGK400
- : 68 m³/hr
- : 5,2 kg/dm<sup>3</sup>
- : 15 km
- : 0 m
- : 5 m/sec
- : 0,0 kPa
- : 27.000 kPa
- : 27.000 kPa

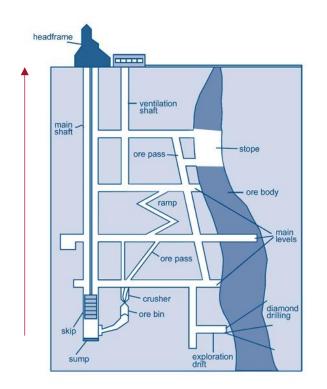




- Slurry pipeline transfer
- Pressure
  - Pipeline length is converted into pressure
  - For a piston diaphragm pump, length of a pipeline is irrelevant
  - A pump does not know how long the pipeline is (and it does not care)
  - A pump does not know what kind of slurry it pumps (and it does not care)



- Slurry pipeline transfer
- Pressure



#### Vertical pipeline (only static head), length 1,8 km, horizontal length is 0, pressure is 20.000 kPa

#### Length of a pipeline is irrelevant!!!



Horizontal pipeline (only friction losses), length 200 km, is pressure is 20.000 kPa





- Piston diaphragm pump selection
- Main criteria for pump size selection:
  - Capacity in m<sup>3</sup>/hr or GPM
  - Pressure in bar, kPa or PSI



- Piston diaphragm pump selection
- Main criteria for pump size selection:
  - Capacity in m<sup>3</sup>/hr or GPM



FELUWA Pumpen GmbH

- Piston diaphragm pump selection
- Pump capacity depends on:
  - Piston volume
  - Number of cylinders
  - Number of pump chambers
  - Pressure/volumetric efficiency
  - Stroke rate
  - Available installed power

JWA Pumpen GmbH

- Piston diaphragm pump selection
- Pump capacity depends on:
  - Piston volume
    - Determined by
      - Surface area of piston
      - Stroke length
      - Formula :  $((0,25 \times \pi \times D^2) \times \text{stroke length})$
      - Example :

- Piston diameter : 3,4 dm
- Piston stroke : 5,0 dm
- Piston volume : 45,4 dm<sup>3</sup>



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Number of cylinders and pump chambers
    - Piston diaphragm pumps are available in various configurations:
      - Simplex single acting (1 cylinder, 1 pump chamber)
      - Simplex double acting (1 cylinder, 2 pump chambers)
      - Duplex double acting (2 cylinders, 4 pump chambers)
      - Triplex single acting (3 cylinders, 3 pump chambers)
      - Quintuplex single acting (5 cylinders, 5 pump chambers)



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Simplex single acting (1 cylinder, 1 pump chamber)
  - Feluwa SG



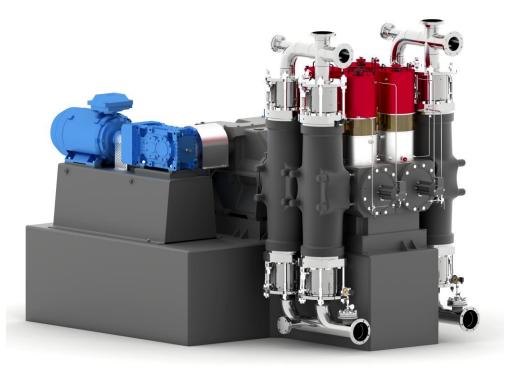


- Piston diaphragm pump selection
- Pump capacity depends on:
  - Simplex double acting (1 cylinder, 2 pump chambers)
  - Feluwa SG

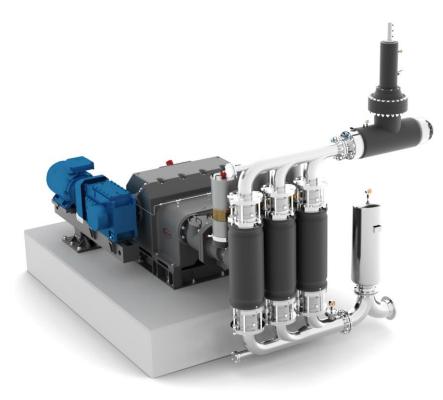




- Piston diaphragm pump selection
- Pump capacity depends on:
  - Duplex double acting (2 cylinders, 4 pump chambers)
  - Feluwa DGK



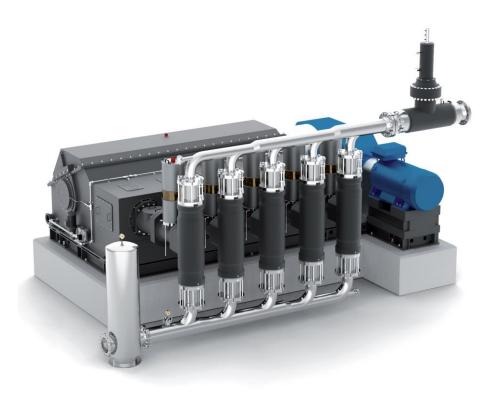
- Piston diaphragm pump selection
- Pump capacity depends on:
  - Triplex single acting (3 cylinders, 3 pump chambers)
  - Feluwa TGK



FELUWA Pumpen GmbH



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Quintuplex single acting (5 cylinders, 5 pump chambers)
  - Feluwa QGK



FELUWA Pumpen GmbH

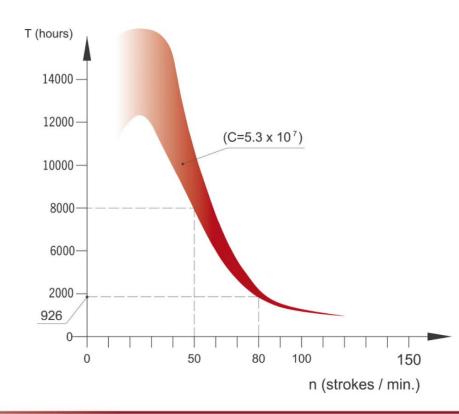
- Piston diaphragm pump selection
- Pump capacity depends on:
  - Pressure/volumetric efficiency
    - Pressure determines the volumetric efficiency
    - The higher the discharge pressure, the lower the volumetric efficiency
    - Criteria
      - Air content (compressibility) in propelling liquid
      - Air content (compressibility) in slurry
      - "Elasticity" of pressure bearing pump components
    - Depending on pressure, volumetric efficiency can be as low as 90%!



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Stroke rate (per minute)
    - For large pumps, stroke rate should be limited to 50 per minute
    - Stroke rate determines
      - Lifetime of valve components
      - NPSHr
      - Smooth and quiet operation
      - Less noise
      - Longer lifetime of pump



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Relationship between stroke rate and valve life



🕽 FELUWA Pumpen GmbH



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Relationship between stroke rate and valve life
    - Relation is not linear but exponential
    - In case stroke rate increases by 10%, valve life is not decreased by 10% but could be 20 or 25% shorter (example)



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Available installed power (in kW)
    - Required power is a function of capacity and pressure
    - Relationship between capacity and pressure is linear
    - If capacity increases by 50% required power will increase by 50% (at the same pressure)
    - Sufficient power has to be installed to handle capacity and pressure



- Piston diaphragm pump selection
- Pump capacity depends on:
  - Formula for capacity
  - (Piston volume x number of cylinders x stroke rate x volumetric efficiency x 60)/1000 = capacity in m<sup>3</sup>/hr
  - Example : (45,3 x 3 x 50 x 90% x 60)/1000 = 367 m<sup>3</sup>/hr



- Piston diaphragm pump selection
- Main criteria for pump size selection:
  - Pressure in bar, kPa or PSI



) FELUWA Pumpen GmbH

- Piston diaphragm pump selection
- Pressure depends on:
  - Rod load of power end
  - Design of pressure bearing components
  - Available installed power

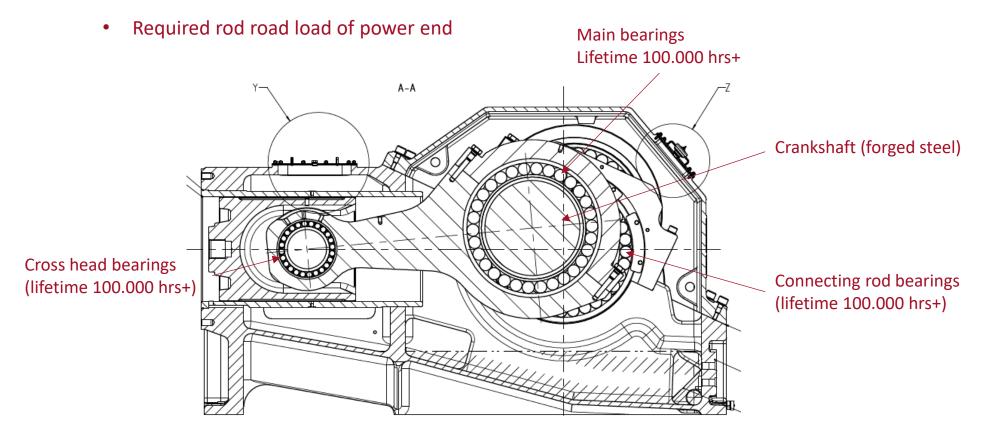
- Piston diaphragm pump selection
- Pressure depends on:
  - Rod load of power end
    - Road load/force is the mechanical capability of the pump to create a force (in kN)
      - The pump power-end is designed with a specific rod load
      - The road load of large slurry transfer pumps is typically 1.000 kN of more
      - The available rod load has to exceed the required rod load, created by the back pressure of the pipeline, pressure vessel, etc.



- Piston diaphragm pump selection
- Pressure depends on:
  - Required road load of power end
    - Determined by
      - Surface area of piston
      - Discharge pressure
      - Formula: ((0,25 x  $\pi$  x D<sup>2</sup>) x discharge pressure)
      - Example :
        - Piston diameter : 3,4 dm
        - Required pressure : 150 bar
        - Required rod load : 1.361 kN



- Piston diaphragm pump selection
- Pressure depends on:

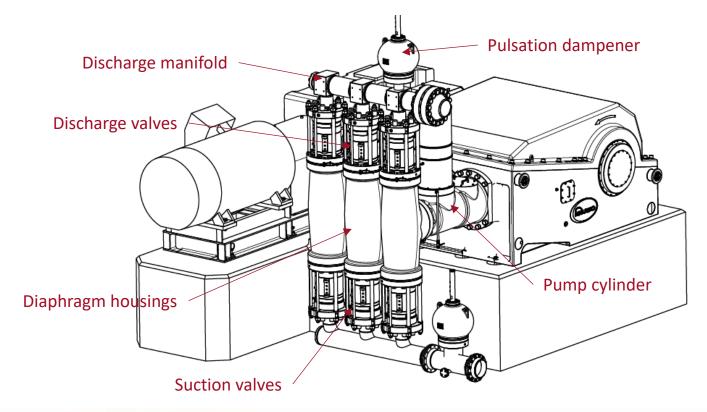


🛛 FELUWA Pumpen GmbH

- Piston diaphragm pump selection
- Pressure depends on:
  - Design of pressure bearing components
    - Pressure bearing components in a piston diaphragm pump are
      - Pump cylinder (in which piston moves back and forward)
      - Suction valves
      - Diaphragm housings
      - Discharge valves
      - Discharge manifold
      - Discharge pulsation dampeners



- Piston diaphragm pump selection
- Pressure depends on:
  - Pressure bearing components in a piston diaphragm pump are



FELUWA Pumpen GmbH

- Piston diaphragm pump selection
- Installed power:
  - Available installed power (in kW)
    - Required power is a function of capacity and pressure
    - Relationship between capacity and pressure is linear
    - If pressure increases by 50% required power will increase by 50% (at the same capacity)
    - Sufficient power has to be installed to handle capacity and pressure



- Piston diaphragm pump selection
- Installed power:
  - Installed power has to exceed required power, depending on:
    - Capacity
    - Pressure
    - Mechanical efficiency
      - Pump (typical 95%)
      - External gearbox (typical 98%)
      - Motor (typical 98 to 95%
    - Altitude (above 1.000 m derating applies)
    - Ambient temperature
    - Service factor (1,0 to 1,25)



- Piston diaphragm pump selection
- Example pump selection process: •

•	Pipeline capacity		: 1.400 m³/hr
•	Discharge pressure		: 150 bar
•	Number of operating pumps		: 4
•	Capacity per pump		: 350 m³/hr
	1)	Select most likely pump	: TGK500 (triplex single acting)
	2) Review volumetric efficiency at 150 bar		: 92%
	3)	Select piston diameter	: 340 mm
	4)	Check rod load at maximum pressure	: 1.361 kN (is below design rod load)
	5)	Required capacity	: 350 m³/hr
	6)	Calculate required stroke rate	: 47/min (is below acceptable maximum)
			TOUEDO

- 7) Confirmation of selected pump
- : TGK500



- Piston diaphragm pump selection
- TGK500



🛛 FELUWA Pumpen GmbH



- Piston diaphragm pump selection
- Example pump selection process:
  - Other selection criteria

•

•

- SG of slurry : for NPSHr
- Viscosity : for NPSHr
- Altitude : for installed power
- Type of valve : cone or ball
  - Valve size : slurry velocity through valve should not exceed 2 m/sec
  - Suction dampener size : peak to peak pulsations should not exceed 3%
- Discharge dampener size
- : peak to peak pulsations should not exceed 3%



- Piston diaphragm pump selection
- Example pump selection process:
  - Other selection criteria
    - Type of slurry (concentrate or tailings) is not a selection criteria!!!





#### **Differences between tailings and concentrate slurry**

© FELUWA Pumpen GmbH

- Differences between tailings and concentrate slurry pipelines
- Concentrate slurry:
  - Destination is refinery (valuable product)
  - Constant solids concentration
  - Constant particle sizes
  - Long pipelines
  - High pressures
  - Lower capacity
- Tailings slurry:
  - Destination is dumpsite (TSF) (valueless product)
  - Varying solids concentration
  - Varying particle sizes
  - Short pipelines
  - Low pressure
  - Higher capacity







- Differences between tailings and concentrate slurry pipelines
- Concentrate slurry:
  - Controlled properties
- Tailings slurry:
  - Less controlled properties
- Tailing slurry is much more demanding and challenging on pumps than concentrate slurry



- ArcelorMittal/Nippon Steel
- Customer : AMNS, Dabuna, India
- Number of pumps : 2
- Application : Iron ore tailings slurry transfer
- Capacity : 636 m<sup>3</sup>/hr
- Pressure : 6.300 kPa
- In operation : 2024





- Nalco
- Customer : Nalco, India
- Number of pumps : 2
- Application : Red mud transfer
- Capacity : 250 m<sup>3</sup>/hr
- Pressure : 13.000 kPa
- In operation : 2024





- Summary
- N.D. Rao (President Amalgam Steel):

"For a pump it does not matter if it handles concentrate or tailings, slurry is slurry" $^{\circ}$ 







- Conclusion:
- A reference in tailings is as good as a reference in concentrate
- A reference in concentrate is as good as a reference in tailings
- Tailing slurry is much more demanding and challenging on pumps than concentrate slurry
- For a piston diaphragm pump it does not matter if it handles concentrate or tailings, slurry is slurry
- Remember



# SLURRY

ELUWA Pumpen GmbH







# SLURRY

ELUWA Pumpen GmbH



### **Questions?**

## Thank you!

### www.feluwa.com

LUWA Pumpen GmbH





# FELUWA Pumps for challenging media.

Safe. Efficient. Environmentally friendly.



🛛 FELUWA Pumpen GmbH